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3 **Extending the use of dewatered alum sludge as a P-trapping material**
4 **in effluent purification: Study on two separate water treatment**
5 **sludges**
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22 **Abstract**

23 The generation of alum sludge from drinking water purification process remains inevitable when
24 aluminium sulphate is used as primary coagulant for raw water coagulation. Sustainable managing
25 such the sludge becomes an increasing concern in water industry. Its beneficial reuse is therefore
26 highly desirable and has attracted considerable research efforts. In view of the novel development of
27 alum sludge as a value-added raw material for beneficial reuse for wastewater treatment, this study
28 examined the maximum phosphorus-adsorption capacity of two dewatered alum sludges sampled
29 from two largest water treatment works in Dublin, Ireland. The objective lies in clarifying the
30 change of alum sludge characteristics and its P-adsorption capacity over the location of the alum
31 sludge produced and the raw water being treated. Experiments have demonstrated that the two alum

32 sludges have the similar P adsorption capacity (14.3mg P/g sludge for Ballymore-Eustace sludge
33 and 13.1 mg P/g sludge for Leixlip sludge at pH 7.0). However, the study supports that alum sludge
34 beneficial reuse as a low cost adsorbent for P immobilization should study its P-adsorption capacity
35 before any decision of large application is made since the raw water quality will affect the sludge
36 characteristics and therefore influence its adsorption ability.

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39 **Keywords** Adsorption; constructed wetland; dewatered alum sludge; phosphorus; reuse;
40 wastewater treatment

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45 **Introduction**

46 On the longer term, beneficial reuse in large scale of industrial wastes/by-products will help to
47 promote the sustainable development. Effective management of the aluminium-coagulated drinking
48 water treatment sludge (commonly termed as alum sludge) requires a sustainable approach that
49 maximizes its value of reuse/recycle for other industrial demands and the environmental needs.
50 Beneficial reuse of the alum sludge seems extremely desirable because it is an easily, locally and
51 largely available by-product inevitably produced from water treatment works worldwide when
52 aluminium sulphate is used as primary coagulant. In Ireland, 18,000 tonnes (dry solids) of alum
53 sludge in an annual basis is generated with landfill disposal costs of about €3.2 million. In the UK,
54 about 182,000 tonnes (dry solids) of waterworks sludge is generated each year, with disposal to
55 landfill as the predominant disposal route. ^[1] Researchers have worked for years to investigate the
56 feasibility of various possible reuse of the alum sludge, but the major route of reuse lies in

57 manufacturing and construction industries. ^[2] The final disposal of the alum sludge is still focused
58 on landfill with little known value of reuse. However, alum sludge is predominantly composed of
59 amorphous aluminium hydroxide. It holds great promise for use as a valuable material or adsorbent
60 in the treatment of wastewater since the aluminium can enhance adsorption and chemical
61 precipitation processes to remove various pollutants, especially phosphorus (P). This is
62 acknowledged from the principle of chemistry that aluminium ion has strong adsorption affinity
63 with P. ^[3]

64

65 In the Centre for Water Resource Research, University College Dublin, Ireland, a research group
66 has conducted extensive work to identify the characteristics and the P adsorption capacity of the
67 locally generated alum sludge. It has been demonstrated that the dewatered alum sludge is a reliable
68 and cost-effective material for P-rich wastewater treatment. ^[4-8] This has provided valuable
69 information regarding a beneficial reuse of the alum sludge in environmental and civil engineering.
70 For example, a so-called novel engineered wetland system for high strength P-rich wastewater
71 treatment has been developed by employing locally dewatered alum sludge as main substrate in the
72 wetland system. ^[9] This provides a good showcase of using “waste” for wastewater treatment. ^[1]

73

74 Although it has been demonstrated that alum sludge exhibited good P adsorption capacity, the
75 capacity is affected by many factors, such as the nature of the alum sludge, which includes (i) the
76 dosage of aluminium sulphate for coagulation and (ii) characteristics of the raw water being treated
77 etc. In addition, these factors often vary from site to site and from year to year. Therefore results
78 obtained from any study of alum sludge adsorption capacity for P immobilization are specific to the
79 particular location and season. For these reasons results of P adsorption obtained from alum sludge
80 adsorption trial in one location cannot be accurately extrapolated for different alum sludges in other
81 locations across the country. Therefore, site- and sludge type-specific information for P adsorption

82 should be obtained by performing controlled laboratory experiments.

83

84 Only in Dublin, there are four water treatment works (WTW) to supply drinking water to the city
85 (Fig. 1). Ballymore-Eustace WTW (located in south Dublin) and Leixlip WTW (located in West
86 Dublin) are the two major waterworks to provide drinking water service. This paper aims at
87 examining P adsorption capacity onto alum sludge by sampling (in the same season) alum sludges
88 derived from two separate WTW in Dublin. Characteristics and P adsorption capacity of the two
89 kinds of alum sludges were examined in detail in a comparative manner. Thereafter, the application
90 prospects of the alum sludge as main substrate in engineered treatment wetland system for P-rich
91 wastewater treatment are also discussed.

92

[Insert Fig. 1 here]

93

94 **Materials and methods**

95 *Alum sludges and their characterization*

96 Dewatered alum sludge cakes of about 10 kg were collected respectively from the dewatering unit
97 of the Ballymore-Eustace WTW (located in Co. Kildare, South Dublin) and Leixlip WTW (located
98 in west Dublin) on the same day in May 2007 (Fig. 1). The former uses a nearby Poulaphuca
99 reservoir water to produce 230,000 m³/d of potable water and the latter extracts the water from
100 River Liffey. The alum sludge in Ballymore-Eustace WTW was the brownish-green residual
101 derived from the treatment of a medium colour, medium turbidity, raw water that had been sourced
102 from the Dublin and Wicklow mountains, which are upland catchments of peat over granite
103 bedrock. The alum sludge in Leixlip WTW was the dark brown residue produced from the
104 treatment of a medium colour, medium turbidity, raw water that had been sourced from the River
105 Liffey, which is originated from the upland catchment of limestone bedrock.

106

107 Both the waterworks use aluminium sulphate as coagulant with dosage of 40-65 mg/L for
108 Ballymore WTW and 40-60 mg/L for Leixlip WTW, respectively, to treat raw waters via the
109 conventional processes of coagulation/flocculation, sedimentation, filtration and disinfection.
110 Currently, in both waterworks, alum sludges from sedimentation tank together with back washing
111 stream from filtration tank were thickened and then conditioned with organic polymer of Magnafloc
112 LT25 with dosage of 0.6-1.5 mg/L for Ballymore WTW and 0.2-1.0 mg/L for Leixlip WTW,
113 respectively. Polymer conditioned sludges were then dewatered by filter press to produce sludge
114 cakes for landfill as final disposal in both the waterworks.

115

116 The collected alum sludge cakes (with solids content of 23% for Ballymore WTW and 25% for
117 Leixlip WTW, respectively) were air-dried and then ground and sieved to prepare the testing
118 samples. The alum sludges were further oven dried at 103 ± 2 °C for examining their physical and
119 chemical properties. Characterization of the sludges was conducted using an energy dispersive
120 spectrometry (EDS, INCA Energy, Oxford Instruments, Oxfordshire, UK). The major elemental
121 components of Al, Fe, Ca, Mg, P and Si of the sludges were obtained by using Inductively Coupled
122 Plasma-Optical Emission Spectrum (ICP-OES, IRIS Intrepid II XSP, Thermo Elemental, Franklin,
123 Massachusetts, USA) while the Cu, Zn, Cd and Pb were determined by using Inductively Coupled
124 Plasma-Mass Spectrometry (ICP-MS, X series, Thermo Elemental, Franklin, Massachusetts, USA).
125 TOC (total organic carbon) was measured by TOC-V_{CSH} (Shimadzu, Tokyo, Japan). The specific
126 surface area of the sludge samples was determined by the SET/N₂-adsorption method.

127

128 ***P-adsorption tests***

129 Series of batch adsorption experimental investigations were conducted on P adsorption behaviour
130 coupled with the adsorption capacity of the dewatered alum sludge determined using the Langmuir
131 isotherm. Its linear form is given in Eq. (1).

132
$$\frac{C_e}{q_e} = \frac{1}{Q_0 b} + \frac{C_e}{Q_0} \quad (1)$$

133 where q_e is defined as the adsorption capacity at equilibrium, (mg P/g), b is a sorption constant
134 related to P binding energy, (L/mg), Q_0 is the maximum adsorption capacity (mg P/g sludge) and C_e
135 is the equilibrium P concentration (mg P/L). The slope and the intercept of the plot of (C_e/q_e) versus
136 C_e give the values of Q_0 and b .

137

138 The phosphorus aqueous solution used for batch adsorption tests were prepared by dissolving
139 potassium dihydrogen phosphate (Riedel De Haen KH_2PO_4 , AnalaR grade) in distilled water. The
140 Langmuir adsorption isotherm was studied by a series of batch adsorption tests. Initially, different
141 weight of prepared alum sludges (with diameter less than 0.063mm) ranging from 0.1g to 0.5 g and
142 100 mL of prepared P solution (with initial P concentration of 100 mg P/L) were poured into
143 150mL plastic bottles. Thereafter, the pH of the mixed suspensions were adjusted to 4.3, 6.0, 7.0,
144 8.5 and 9.0, respectively, by adding 0.1M sulphuric acid and 0.01M sodium hydroxide. The mixed
145 samples were then placed on a Stuart Orbital Shaker (SSL 1, Bibby Sterilin Ltd.) and agitated at
146 200 rpm for 48 hours for equilibrium to be achieved. This equilibrium time has been determined in
147 a previous study.^[4] After 48 hours, the samples were removed from the shaker and filtered using a
148 0.45 Millipore membrane filters to separate the solids from the liquid for P residual monitoring,
149 which was conducted using the stannous chloride method (4500-PD)^[10] via a Unicam Helios α
150 spectrophotometer (Helios Alpha, Unicam Ltd., Cambridge, UK). Duplicable tests were applied for
151 P adsorption tests and the results were very close. Therefore, the average value was reported in the
152 paper.

153

154 **Results**

155 *Alum sludge characterization*

156 The energy dispersive spectrometry spectra of the sludges are shown in Fig. 2. The chemical
157 components have been clearly identified and Table 1 lists each of them in mass percentage. As
158 expected, the main metallic element presented in both the sludges was Al, which was 17% (in mass)
159 in Ballymore-Eustace sludge and 22% in Leixlip sludge, respectively. The other principal chemical
160 components were Ca, Fe and Si and the amount was <3% in mass for both the sludges. The metallic
161 elements of Cu, Zn, Cd and Pb in both the sludges are extremely low. It is noted that both the
162 sludges contained significant amount of organic matters including humic acid. The amount given in
163 terms of TOC is 173 mg/g-sludge for Ballymore-Eustace sludge and 118 mg/g-sludge for Leixlip
164 sludge, respectively. In addition, both the sludges contained inherent P especially for Leixlip
165 sludge, given P of 4.2 mg/g-sludge.

166

167 The results of the specific surface area of the sludges showed that the Ballymore-Eustace WTW
168 sludge has specific surface area of 49.03 m²/g-sludge, while the specific surface area of the Leixlip
169 WTW sludge is 46.33 m²/g-sludge.

170

171 **[Insert Fig. 2 here]**

172 **[Insert Table 1 here]**

173 ***Maximum P-adsorption capacity***

174 The maximum P-adsorption capacity of the alum sludges studied is given in Table 2. It shows that
175 the dewatered alum sludges possess excellent P-adsorption capability with P-adsorption favoured at
176 lower pH. The highest P adsorption capacity tested is 22.4 mg P/g sludge (at pH=4.3) for
177 Ballymore-Eustace sludge and 20.1 mg P/g sludge (at pH=4.3) for Leixlip sludge, respectively.
178 Comparatively, the Ballymore-Eustace sludge has higher adsorption capacity in the lower pH range
179 than that of the Leixlip sludge despite its lower Al content (see Table 1). However, the Leixlip
180 sludge exhibited higher P-adsorption capacity when the pH of the P solution exceeded 7.0.

181 **[Insert Table 2 here]**

182 **Discussion**

183 Globally the water industry is estimated to be worth €370Bn per annum. The Irish water industry is
184 estimated to be worth €1.5Bn per annum. There are strong drivers for continued growth and
185 innovation in this industry due to the urbanization, population growth and economical development.
186 In view of the water industry development, beneficial reuse of alum sludge is an emerged area in
187 environmental sustainable research and application. Alum sludges derived from the two largest
188 water treatment works in Dublin were studied for possible variability of their maximum P-
189 adsorption capacity, which may be linked with the sludge characteristics.

190
191 It is noted that, for the two alum sludges studied, there is no significant difference in maximum P-
192 adsorption capacity being observed (Table 2). As a whole, the two Irish dewatered alum sludges
193 exhibited an excellent P-adsorption ability, which is capable to compare with other alum sludges
194 produced in other places in the world ^[6,11,12] and even other industrial by-products/materials used
195 for P adsorption.^[13,14] However, Ballymore-Eustace sludge has high P-adsorption capacity (in acid
196 environment) (Table 2) while its Al content is lower than that of Leixlip sludge (Table 1). This
197 result seems to be hard to understand since the P-adsorption depends largely on the Al content in
198 the sludge via ligand exchange.^[5] Actually, it is noted from Table 1 that the P and Ca contents in
199 Leixlip sludge are significantly higher than those in Ballymore-Eustace sludge. The high P, Ca
200 content in Leixlip sludge may cause the low ability of P-adsorption as investigated previously by
201 Yang et al.^[5] In addition, TOC content in Ballymore-Eustace sludge is obviously high compared
202 with that in Leixlip sludge. The high TOC content may affect the P adsorption since the P
203 adsorption by alum sludge is dominated by the significant amount of reactive functional groups,
204 such as -OH, -Cl, -SO₄ and humic substances in the sludge surface via the ligand exchange
205 mechanism.^[5] Thus, it is reasonable to believe that the source water quality will affect the sludge

206 characteristics and accordingly affect the P-adsorption capacity.

207

208 The surface area of the two sludges tested indicated that the Ballymore-Eustace sludge has large
209 surface area, which is contribute to the high P adsorption capacity. In general, both the sludges have
210 the surface areas, which are similar in order to that of 61-67 m²/g for water treatment sludge
211 reported by Lee et al. ^[15] It has been pointed out that Ballymore-Eustace sludge contains higher
212 organics (TOC) than that of the Leixlip sludge. This is probably due to the nature of source water
213 quality since the Ballymore-Eustace WTW uses reservoir water, which may contain higher amount
214 of humic substances especially in summer period to promote the possible eutrophication. As such, it
215 is reasonable to infer that the P adsorption capacity of Ballymore-Eustace sludge may be varied
216 cross the season.

217

218 In view of the reuse of the sludges tested as low-cost adsorbents, it is essential that materials are
219 considered as inert, rather than toxic material. The metallic elements of Cu, Zn, Cd and Pb in both
220 the sludges are extremely low and several orders of magnitude below USEPA regulatory guidelines
221 for toxic wastes. ^[16] This reflects a lack of heavy metal contamination in the raw/source waters
222 being treated and suggests that the sludges can be readily used as adsorbents. Bearing this in mind,
223 to develop the alternative options regarding the alum sludge final disposal and beneficial reuse,
224 application of dewatered alum sludge in constructed wetland for P-rich wastewater treatment has
225 been proactively studied in University College Dublin, Ireland. As dewatered alum sludge can play
226 the multi-role in constructed treatment wetland system as low cost adsorbent to enhance P
227 immobilization and as carrier for biofilm attachment/development, the novel alum sludge-based
228 constructed wetland system has been developed, which provides good promise to promote the
229 pollutants treatment efficiencies to a high level.^[1,9]

230

231 **Conclusions**

232 Dewatered alum sludge from two major water treatment works in Dublin, Ireland were sampled and
233 tested for maximum P-adsorption capacity for the purpose of examining the possible variability of
234 the P-adsorption ability. Although there is no significant change on maximum P-adsorption capacity
235 (14.3mg P/g sludge for Ballymore-Eustace sludge and 13.1 mg P/g sludge for Leixlip sludge at pH
236 7.0), the study supports that the raw water quality will affect the sludge characteristics and therefore
237 influence its adsorption ability. As a result, alum sludge beneficial reuse as a low cost adsorbent for
238 P immobilization should study its P-adsorption capacity before any decision of large application is
239 made.

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302 Table 1. The chemical components of the dewatered alum sludge (DAS)

Chemical composition	Unit	Ballymore-Eustace sludge	Leixlip sludge
Al	mg/g DAS	169.52	222.79
P	mg/g DAS	0.582	4.156
Ca	mg/g DAS	4.03	32.73
Fe	mg/g DAS	6.65	6.59
Mg	mg/g DAS	0.251	0.71
Pb	mg/g DAS	0.019	0.021
Cd	µg /g DAS	0.51	0.53
Zn	mg/g DAS	0.065	0.072
Cu	mg/g DAS	0.069	0.039
Si	mg/g DAS	3.11	6.54
TOC	mg-C/g DAS	172.6	117.8

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314 Table 2. The maximum P-adsorption capacity of the DAS studied

pH of P- solution	Ballymore-Eustace sludge (mg-P/g DAS)	Leixlip sludge (mg-P/g DAS)
4.3	22.4	20.1
6.0	18.3	17.0
7.0	14.3	13.1
8.5	1.1	2.8
9.0	0.9	1.6

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329 **Figure caption:**

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331 Fig. 1 Geographic layout of water treatment works in Dublin, Ireland

332 Fig. 2 Energy dispersive spectrometry spectra of the alum sludges; Ballymore-Eustace WTW
333 sludge (left) and Leixlip WTW sludge (right)

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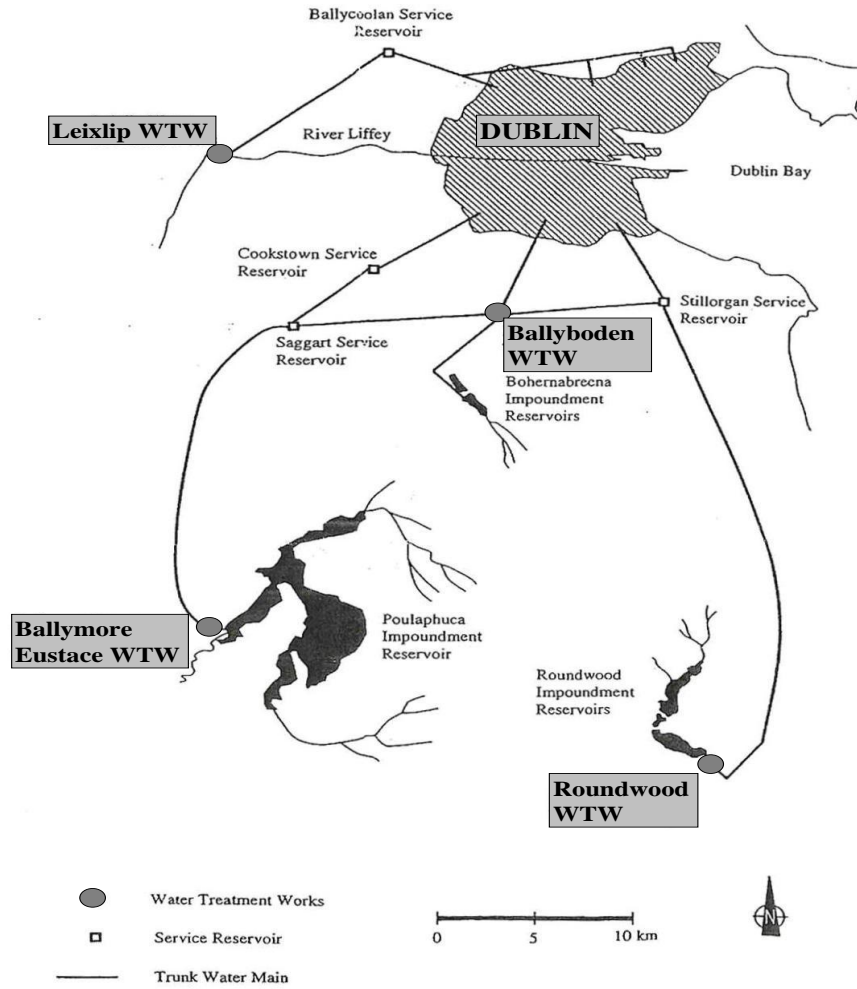
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Fig. 1

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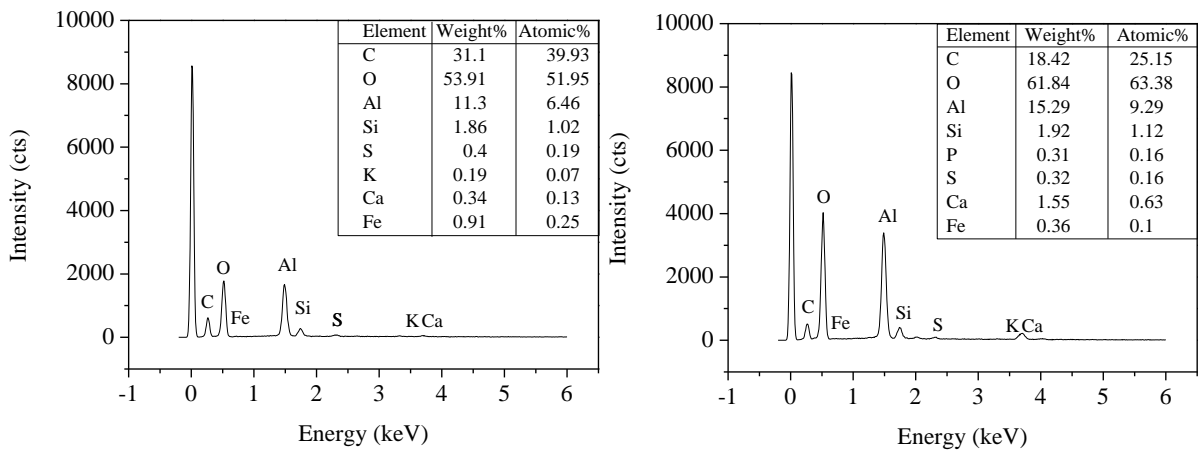
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Fig. 2

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