Polysaccharides from macroalgae: recent advances, novel technologies and challenges in extraction and purification

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Abstract

Polysaccharides obtained from macroalgae have promising prospects both at research and industrial level, and could contribute greatly to the future of marine based bio-economy. Specifically, laminarin and fucoidan from brown macroalgae have a wide variety of potential industrial applications including functional foods, nutraceuticals, pharmaceuticals and cosmeceuticals due to their broad range of biological activities both in vitro and in vivo. These beneficial biological activities are related to the chemical composition and structure of the macroalgal polysaccharides. The molecular weight, monosaccharide composition and sulphate content of these polysaccharides could be influenced by both macroalgal biology (variations in polysaccharide composition due to macroalgae species and their biological cycle) and different extraction/purification techniques employed to obtain polysaccharide enriched products (i.e. de-sulphation or fragmentation of sulphated polysaccharides). This review focuses on the extraction and purification methods for laminarin and fucoidan macroalgal polysaccharides used in the recent literature. The application of innovative extraction technologies (such as ultrasound, microwave and enzyme-assisted extractions), as well as new purification techniques (i.e. membrane separation), are also discussed together with the challenges concerning molecule structure-function relationship and macroalgae variability.

Keywords: seaweed; bioactivity; fucoidan; laminarin; extraction; purification; innovative technology
1. Introduction

Macroalgae are a large and diverse group of marine organisms with more than 10,000 different species described to date (Collins, Fitzgerald, Stanton, & Ross, 2016). Marine macroalgae are able to adapt to the changing and extreme marine environmental conditions i.e. salinity, temperature, nutrients, radiation and combination of light and oxygen concentration by producing unique secondary metabolite compounds including polysaccharides (Collins et al., 2016; Rajauria, Jaiswal, Abu-Ghannam, & Gupta, 2010). These macroalgal polysaccharides, particularly fucoidan and laminarin, show a wide range of biological activities such as antiinflammatory, antimicrobial, anticoagulant, antiadhesive, antioxidant, antiviral, antipeptic, antitumour, antiapoptosis, antiproliferative and immunostimulatory in *in vitro* and *in vivo* model systems (Cong et al., 2016; Jin, Zhang, Wang, & Zhang, 2013; Kadam, Tiwari, & O'Donnell, 2015; Lim et al., 2014; Menshova et al., 2015; Moroney, O'Grady, O'Doherty, & Kerry, 2012; Ngo, Wijesekara, Vo, Van Ta, & Kim, 2011; Roohinejad et al., 2016; Smith et al., 2011)

A representation of the chemical structure of laminarin from *Laminaria digitata* proposed by Adamo et al. (2011) is presented in Figure 1. Laminarin was described as 1,3-linked β-d-glucose residues with different degrees of branching at β-(1,6) that influence the water solubility of the molecules (Rioux, Turgeon, & Beaulieu, 2010). The structure composed of (1,3)-β-D-glucopyranose residues consisting some 6-O-branching (in the main chain) and β-(1,6) (intrachain links). The laminarin structure may vary in degree of branching, the degree of polymerization and the ratio of (1,3)- and (1,6)-glycosidic bonds. They are uncharged molecules at neutral pH which are stabilized by inter-chain hydrogen bonds, thus unable to hydrolyse in the upper gastrointestinal tract and are classified as dietary fibers (O’Sullivan et al., 2010). Laminarins are energy reserve polysaccharides present in reserve vacuoles inside
the macroalgal cell and may constitute up to 35% of the dried weight of the macroalgal biomass (Kadam, Tiwari, et al., 2015).

The chemical structure of fucoidan from *Laminaria saccharina* proposed by Cumashi et al. (2007) is shown in Figure 1. Fucoidan or fucose-containing sulphated polysaccharides have a backbone of (1→3)-linked α-l-fucopyranosyl or alternating (1→3)- and (1→4)-linked α-l-fucopyranosyl residues, but also include sulphated galactofucans with backbones built of (1→6)-β-d-galacto- and/or (1→2)-β-d-mannopyranosyl units with fucose or fuco-oligosaccharide branching, and/or glucuronic acid, xylose or glucose substitutions (Ale, Mikkelsen, & Meyer, 2011b). The l-fucopyranose residues may be substituted with sulphate on C-2, C-4 and rarely on C-3 positions (Ale, Mikkelsen, & Meyer, 2011a). Fucoidans are an integral part of the cell walls and intercellular spaces in brown macroalgae, playing a crucial role in the protection of the macroalgae against the effects of desiccation when the biomass is exposed at low tide (Ale, Mikkelsen, et al., 2011b; Senthilkumar, Manivasagan, Venkatesan, & Kim, 2013).

There is a marked relationship between the chemical structure of both macroalgal polysaccharides (i.e. molecular weight, monosaccharide composition, sulphate content and position) and their biological activity. These differences could be attributed to factors such as macroalgae species, parts of the macroalgae sampled and differences in polysaccharide content and composition depending on the season (Kim, 2012; Men'shova et al., 2012; Skr iptsova, Shevchenko, Tarbeeva, & Zvyagintseva, 2011). Furthermore, it was also observed that structural modifications to these molecules (i.e. molecular weight, degree of sulphation) can occur during the processes of extraction and purification; for instance, use of different extraction solvents and experimental conditions (such as pH, time, temperature and pressure) (Ale, Mikkelsen, et al., 2011a; Foley, Szegedzsi, Mulloy, Samali, & Tuohy, 2011; Hahn, Lang, Ulber, & Muffler, 2012; Lorbeer, Lahnstein, Bulone, Nguyen, & Zhang, 2015).
Therefore, for the extraction and purification of different fractions of laminarin and fucoidan, details on the macroalgal biomass used as well as the methodology followed are extremely important to achieve the bio-activities required as well as complying with good manufacturing practices. The lack of standardized extraction methodologies has prevented the approval of polysaccharides or their derived fractions to be officially approved for pharmaceutical, dermatological, nutraceutical or other commercial applications to date (Ale & Meyer, 2013).

Thus, the present review focuses on the extraction and purification techniques of laminarin and fucoidan from macroalgae described in the recent literature. New processes, technologies and optimized extraction and purification procedures are reported together with the challenges concerning molecule structure-function relationship and macroalgal variability.

2. Extraction of polysaccharides from macroalgae

The process of extraction of macroalgal polysaccharides could include several steps summarized in Figure 2. These extraction steps include preparation of the macroalgal biomass, pre-treatments of the macroalgae, extraction techniques (traditional solvent extraction and innovative technologies) and purification techniques to obtain the polysaccharides of interest and proceed to test its biological activity and potential industrial uses.

2.1 Preparation of macroalgal biomass

The procedure for the extraction of polysaccharides from macroalgae involves cleaning of macroalgae with either sea water or distilled water to remove sand and epiphytes and then drying (oven-drying or freeze-drying). The dried biomass is then milled to obtain the highest
surface-to-volume ratio during the latter extraction procedures (Hahn et al., 2012; Imbs, Ermakova, Malyarenko, Isakov, & Zvyagintseva, 2016).

As an alternative to drying processes, Hjelland, Andersen, and Yang (2012) patented the exudate method to obtain laminarin and fucoidan at commercial amounts from live macroalgal tissue. Using this technique, the fresh macroalgae was cut in pieces of ≥1 cm and piled in a dark-humid place to obtain the exudate from the live macroalgae tissue. After this step, the polysaccharides laminarin and fucoidan could be extracted and purified from the exudates obtained.

2.2. Pre-treatment of macroalgae

Different pre-treatments applied to the dried biomass, together with the detailed description of the extraction techniques described in the recent literature are presented in Table 1. The most commonly performed pre-treatments in the literature were washing of the dried biomass with a mixture of methanol, chloroform and water (4:2:1; v/v/v) (Ale, Maruyama, Tamauchi, Mikkelsen, & Meyer, 2011; Lim et al., 2014), or with acetone alone (Dore et al., 2013). However, a mixture of acetone and ethanol (Shan et al., 2016) or one or several ethanolic pre-treatments at different temperatures have also been applied recently (Imbs et al., 2016; Yuan & Macquarrie, 2015). These alcohol treatments were applied to remove lipids (defatted), proteins (deproteinated) and phenols (dephenolated), but also mannitol and chlorophyll, compounds that are highly bound to the polysaccharides, contaminating the target compounds (Hahn et al., 2012). Other novel pre-treatments recently described in the literature include compressional-puffing-hydrothermal process consisting of heating at atmospheric pressure (140°C, 180°C and 220°C), followed by rapid reduction of pressure in a vessel containing superheated water, which allows the modification of the cellular structure of the macroalgae prior to extraction of fucoidan (Huang, Wu, Yang, Kuan, & Chen, 2016).
2.3. Extraction techniques of polysaccharides

2.3.1. Solvent extraction

The extraction of macroalgal polysaccharides is mainly carried out by solvent extraction, with a wide variation in the conditions and methods used in the literature to date as seen in Table 1. The extraction of macroalgal polysaccharides is typically performed using pretreated dried macroalgae or defatted biomass with different solvents at different temperatures ranging from room temperature to 120°C, for several hours. The most commonly used solvents are water (Cong et al., 2016; Cong, Xiao, Liao, Dong, & Ding, 2014; Shan et al., 2016; Vijayabaskar, Vaseela, & Thirumaran, 2012; J. Wang, Wang, Yun, Zhang, & Zhang, 2012; P. Wang et al., 2012) and ethanol (Foley et al., 2011; Huang et al., 2016). Slightly acidic solutions, i.e. low molarity solutions of HCl have also been described (Anastyuk, Shevchenko, Dmitrenok, & Zvyagintseva, 2012; Dinesh et al., 2016; Imbs et al., 2016; Lorbeer et al., 2015; Menshova et al., 2015).

Following the initial extraction, the solution containing mixed polysaccharides is treated to obtain the specific compounds of interest. One of the main polysaccharide residues at this stage are alginates. Alginates – composed of consecutive mannuronate residues (M-blocks), consecutive guluronate residues (G-blocks), or alternate mannuronate and gulurionate residues (MG-blocks) – show gelation properties in the presence of Ca$_2^+$ or Mn$_2^+$. The 2 ions interact with the anionic polymers containing carboxylate groups through chemical binding, mainly to the stiffer guluronate chains (Assifaoui et al., 2015). Therefore, CaCl$_2$ solutions are normally used in the recent extraction protocols to eliminate the alginates from the mixture containing polysaccharides (Cong et al., 2016; Dinesh et al., 2016; Yuan & Macquarrie, 2015). Other authors described the use of CaCl$_2$ solutions at different concentrations and temperatures as an alternative to the initial water or slow acidic conditions to obtain alginates, laminarin and
fucoidan in a single step and separate them further by applying several consecutive purification steps (Lim et al., 2014).

After the initial solvent extraction, the application of organic solvents (i.e. ethanol) or tensids (cetyltrimethylammonium bromide) are common practices to precipitate the polysaccharides from the mixture (Hahn et al., 2012; Kadam, Tiwari, et al., 2015). The precipitated polysaccharides can then be dialyzed or precipitated further with ethanol in one or several steps to remove salts and other compounds from the enriched extract. Laminarin and fucoidan were further purified from the extract using different techniques such as membrane filtration or chromatographic procedures (Ale, Mikkelsen, et al., 2011a; Cong et al., 2016; Cong et al., 2014).

2.3.2. Innovative extraction technologies

Innovative or novel technologies have been used to develop extraction processes more efficient in terms of yield, time and cost and more environmentally friendly by lowering the energy consumption (Kadam, Tiwari, & O’Donnell, 2013; Barba, Grimi, & Vorobiev, 2015). Extraction technologies such as ultrasound-assisted extraction (UAE), microwave-assisted extraction (MAE) and enzyme-assisted extraction (EAE) have been used to extract macroalgal polysaccharides and other marine bioactive compounds.

Ultrasound-assisted extraction

Ultrasound-assisted extraction has been utilized to extract a number of functional ingredients from multiple plant sources (C Chen, You, Abbasi, Fu, & Liu, 2015; Roselló-Soto et al., 2015; Xu, Zhang, Yang, Song, & Yu, 2015; Ying, Han, & Li, 2011), microalgae (Barba et al., 2015; Parniakov, Apicella, et al., 2015; Parniakov, Barba, et al., 2015) and macroalgae such as phycoerythrin (Le Guillard et al., 2015) and amino acids (Romarís-Hortas, Bermejo-
Barrera, & Moreda-Piñeiro, 2013). UAE was used to obtain polysaccharides from algae (Wijesekara, Pangestuti, & Kim, 2011) and laminarin from Laminaria hyperborea and Ascophyllum nodosum in combination with weak acid solutions (Kadam, Tiwari, et al., 2015). The technology has also been used to breakdown already extracted polysaccharide fractions. The small molecular weight molecules generated during this process showed promising biological and physico-chemical properties than those described in its original conformation in the algae (Sun, Wang, & Zhou, 2012).

UAE is a non-thermal extraction technique wherein sound waves migrating through a medium, inducing pressure variations and cavitations that grow and collapse, transforming the sound waves into mechanical energy, which disrupts the cell walls, reduce the particle size and enhance the contact between the solvents and the targeted compounds (Michalak & Chojnacka, 2014; Ying et al., 2011). Despite being an energy input extraction method, UAE has certain advantages over conventional solvent extraction methods. UAE is cost-effective in comparison with other novel extraction techniques and has high possibilities to scale up to industry. Other advantages of UAE include low solvent consumption, high level of automation, and possibilities to combine this technique with others – i.e. superfluid assisted extraction or microwave-assisted extraction (Ibañez, Herrero, Mendiola, & Castro-Puyana, 2012; Michalak & Chojnacka, 2014).

**Microwave-assisted extraction (MAE)**

Microwave-assisted extraction (MAE) has been used to extract multiple compounds of interest from both plants (Mendes et al., 2016) and algae (Gilbert-López, Barranco, Herrero, Cifuentes, & Ibáñez; Michalak & Chojnacka, 2014). MAE technology was used to extract fucoidan from macroalgae Fucus vesiculosus (Rodriguez-Jasso, Mussatto, Pastrana, Aguilar, & Teixeira, 2011), Undaria pinnatifida (Quitain, Kai, Sasaki, & Goto, 2013) and
Ascophyllum nodosum (Yuan & Macquarrie, 2015) showing yields of fucoidan similar to those obtained with conventional techniques (Rodriguez-Jasso et al., 2011; Yuan & Macquarrie, 2015). However, effect of the microwaves on the structural properties and bioactivity of fucoidan is still unknown. Some studies used MAE on previously extracted fucoidans from sporophylls of Undaria pinnatifida to produce more valuable low-molecular-weight products of around 5-30 kDa (You, Yang, Lee, & Lee, 2010).

This extraction technology, a thermal based approach, uses microwaves causing temperature rise and water evaporation of intracellular fluids that leads to break down of the cell walls, thus release the intracellular compounds into the medium (Michalak & Chojnacka, 2014). Compared to the ultrasounds, MAE is an energy-assisted extraction method, uses lower amounts of solvents and improved the extraction yields of certain intracellular compounds. However, the heat generated during the extraction process might cause damages to heat-sensitive compounds (Michalak & Chojnacka, 2014).

**Enzyme-assisted extraction (EAE)**

Enzyme-assisted extraction is a promising alternative to the conventional solvent based methods, due to its high catalytic efficiency, high specificity, and mild reactive conditions (Kulshreshtha et al., 2015). Additionally, the enzymes used are eco-friendly, non-toxic, food grade and could be used in large scale operations (Michalak & Chojnacka, 2014). However, the usage of enzymes is limited due to their high price in industrial applications (Hahn et al., 2012; Michalak & Chojnacka, 2014).

Enzyme-assisted extraction (EAE) was used in macroalgae to enhance the extraction of several targeted compounds such as proteins and phenols (T. Wang et al., 2010), carotenoids and lipids (Billakanti, Catchpole, Fenton, Mitchell, & MacKenzie, 2013). The use of protease enzymes was described for the isolation of fucoidan with anticoagulant, antithrombotic,
antioxidant and antiinflammatory effects from *Sargassum vulgare* biomass followed by solvent precipitation with acetone (Dore et al., 2013). Recently, the use of a combination of carbohydrase and protease enzymes resulted in the extraction of potent antiviral compounds from brown algae *Chondrus crispus* and *Codium fragile* (Kulshreshtha et al., 2015). This innovative technology relies on the application of one or several enzymes that interact with its substrates under particular conditions defined by each enzyme, which help the extraction of particular compounds by degrading the cell wall. Macroalgae cells are chemically and structurally more complex than the terrestrial plants. The application of a well-defined enzyme mixture and the optimal conditions (mainly pH and temperature) for enzymatic activity, are the main parameters to obtain a good recovery of the compounds of interest (Jeon, Wijesinghe, & Kim, 2011). Jeon et al. (2011) has described the optimum conditions of pH (ranging from 3.8 to 8) and temperature (from 40 to 60°C) for enzymes such as amyloglucosidase (AMG), agarase, alcalase, carragenanase, cellucast, cellulose protamex, kojizyme, neutrase, termamyl, ultraflo, umamizyme, xylanase and viscozyme which are most commonly used in EAE.

### 3. Purification techniques

After the process of extraction, the polysaccharides are dissolved in a rich mixture (with variable monosaccharide composition and sulphate contents), together with small amounts of proteins and phenolic compounds that could also display several beneficial biological activities both *in vitro* and *in vivo* (Ale, Mikkelsen, et al., 2011b). Before the bioactivity tests, the polysaccharide mixture usually undertakes one or more processes of purification to further enrich the extracts with the polysaccharides of interest (Jin et al., 2013; P. Wang et al., 2012). The most commonly used techniques in polysaccharide purification are ion-
exchange chromatography (IEC), size-exclusion chromatography (SEC), affinity chromatography and membrane filtration.

3.1. Ion-exchange chromatography (IEC)

Ion-exchange chromatography (IEC) is an established technique used in the separation of charged molecules across a breadth of applications and industries. The separation of the compounds achieved with IEC is based on the adsorption of charged solute molecules on to immobilized ion exchange groups of opposite charge and its elution by changing the concentration or pH of the running buffer (Rieman & Walton, 2013). The high performance and resolution showed by AEC, together with its relatively low average cost, large sample handling capacity and automation made this technique one of the most widely used liquid chromatography technique for purification (Acikara, 2013).

Positively charged ion exchange resin with affinity for molecules with net negative surface charges (anion-exchange chromatography (AEC)) are commonly used in sulphated polysaccharide purification. Fucoidans exhibit high anionic charges, even at low pH values, due to the sulphate ester groups linked to the carbohydrate backbone. Thus, AEC is one of the most common purification techniques used under different experimental conditions (Table 2). The elution of the adsorbed fucoidan from different resins was performed by stepwise (Anastyuk, Imbs, Shevchenko, Dmitrenok, & Zvyagintseva, 2012; Cong et al., 2016) or linear (Dinesh et al., 2016; Imbs et al., 2016; Menshova et al., 2015; J. Wang et al., 2012) NaCl salt gradient. Different fucoidan fractions could be further separated by AEC based on the degree of sulphation of the molecules. In general, highly sulphated fucoidan fractions showed stronger interactions with the resins, which require higher salt concentrations to elute these compounds. Thus, AEC could be used to purify different fucoidan fractions from macroalgae that exhibit distinct structural and chemical properties (Hahn et al., 2012).
3.2. Size-exclusion chromatography (SEC)

Size-exclusion chromatography (SEC) is used to separate the molecules based on their size as they pass through a porous matrix of particles with chemical and physical stability and inertness. Unlike IEC, molecules do not bind to the chromatography medium in SEC thus, the buffer composition does not directly affect the degree of separation between the peaks. Subsequently, a significant advantage of SEC is that it can be used directly after IEC or other purification techniques using the buffer that better suits the type of sample in terms of preservation or further purification (Mori & Barth, 2013). As seen in Tables 2 and 3, the application of SEC after IEC is a common procedure in the purification of polysaccharides. Different SEC conditions used for polysaccharide purification in the recent literature are compiled in Table 3. During this purification step, different single columns such as Sepharose CL-6B, PL aquagel-OH, Sephacryl S-300 or Superdex 200 (Cong et al., 2016; Huang et al., 2016; P. Wang et al., 2012), or columns successively connected i.e. TSK G4000 SW-XL and TSK G3000 SW-XL (Anastyuk, Imbs, et al., 2012; Foley et al., 2011; Imbs et al., 2010) were used. The application of SEC allows fractionation of the laminarins and fucoidans according to their molecular weights. Furthermore, it can also help in desalting the purified compounds from the high salt concentrations, a major step during AEC purification (Hahn et al., 2012).

3.3. Affinity chromatography

Affinity chromatography is based on the reversible interaction between the molecules and a specific ligand coupled to a chromatography matrix, enabling the purification of different compounds on the basis of its biological function or individual chemical structure (Dunlap, 2013). For instance, the use of immobilized dyes (dye-affinity chromatography) to specifically bind different proteins from other cellular crude extracts is a common practice in the process of protein purification (Janson, 2012).
In the case of polysaccharides, fucose-binding lectins were used effectively to purify fucoidan from crude solutions; however problems could arise if the sulphate content of the polysaccharide blocks the fucose units that interact with the lectins (Hahn et al., 2016). Strong interactions have been appreciated between the anionic sulphate esters of the sulphated polysaccharides and different cationic dyes (i.e. toluidine and methylene blue), forming a strong donor-acceptor complex (Hahn et al., 2016). Recently, Hahn et al. (2016) developed a new dye-affinity chromatography method using modified amino-derivatized sephabeads with toluidine blue, showing promising results in the purification of fucoidan from brown macroalgae at higher purity levels than the commercially available purified fucoidan from Sigma-Aldrich (95%).

3.4. Membrane filtration

Novel technologies, such as membrane filtration, are used to obtain polysaccharide fractions based on the molecular weight of the molecules of interest. Authors in the recent literature used one or several steps of filtration and/or dialysis of the polysaccharide mixture with different molecular weight cut off (MWCO) membranes/filters mainly to remove salts from the extracts (Anastyuk et al., 2010). The use of MWCO membranes to separate laminarin from fucoidan and/or fractionation of the different polysaccharides from macroalgae is barely described (Hjelland et al., 2012). However, membrane separation methods have been successfully applied in other fields i.e. separation of milk components (Costa, Elias-Argote, Jiménez-Flores, & Gigante, 2010), extraction and concentration of bacterial extra-cellular polysaccharides (Wingender, Neu, & Flemming, 2012) and hydrosoluble polysaccharides from terrestrial plants (Wan, Prudente, & Sathivel, 2012) and microalgae origin (CS Chen et al., 2011; Marcati et al., 2014; Mezhoud et al., 2014; Patel et al., 2013).
Filtration techniques seem well suited for initial extraction and purification steps at industrial scale as they can be automatized and allow the separation of large volumes of solutions (Patel et al., 2013). However, their widespread applications have been hindered due to excessive membrane fouling (which could result in reduced performance), high energy inputs and frequent membrane cleaning or replacement (Marcati et al., 2014). Nevertheless, to improve the efficiency of membranes in the separation of different compounds of interest and to avoid fouling, both tangential flow filtration (diafiltration) (Patel et al., 2013) or a combination of sequential ultrafiltration and diafiltration with membranes with decreasing MWCO (Marcati et al., 2014) have been proposed.

4. Optimization of the methods

As described in sections 2 and 3, there are many protocols proposed for the extraction of polysaccharides, however, there is a need to optimize the different conditions of the extraction processes to obtain the best possible response. Traditionally, the optimization in analytical chemistry has been carried out by studying “one-variable-at-a-time”. In this optimization strategy, the conditions of one parameter were changed while the others remained constant (Bezerra, Santelli, Oliveira, Villar, & Escaleira, 2008). This optimization technique is time- and cost-consuming and does not include the interactive effects among the variables studied (Bezerra et al., 2008; Roselló-Soto et al., 2015).

To solve these problems, response surface methodology (RSM), a multivariate statistic technique, has been considered the most relevant in analytical optimization. RSM is based on the fit of a polynomial equation to the experimental data with the objective of making statistical previsions. RSM could include first-order models (i.e. when the data does not present curvature), and more commonly experimental designs such as three-level factorial, Box-Behnken, central composite and Doehlert designs. Box-Behnken design is an efficient
and economical design when dealing with large number of variables (Bezerra et al., 2008; Roselló-Soto et al., 2015) with the advantage that only 3 levels per factor are included in the model. However, the confidence interval of this design is broader in comparison to central composite designs (Hahn et al., 2012).

The yield and chemical structure of polysaccharides (i.e. molecular weight, sulphate content etc) could be affected by different factors (such as pH, temperature, time, pressure and sample to solvent ratio) used during extraction. Therefore, it is essential to optimize at least some critical factors that could directly affect the extraction of polysaccharides during multi-step extraction processes (Hahn et al., 2012). Studies on the optimization of one or more steps of the extraction processes of polysaccharides from macroalgae mainly used Box-Behnken and central composite designs to analyse at least 3 or more factors affecting the extraction process (Ale, Mikkelsen, et al., 2011a; Hifney, Fawzy, Abdel-Gawad, & Gomaa, 2016; Lorbeer et al., 2015).

Ale, Mikkelsen, et al. (2011a) optimized one step process of fucoidan extraction from Sargassum sp. using a central composite design. The model took 3 factors (molarity, temperature and time) into account when extracting fucoidan from the original dried-milled biomass with HCl solution. The authors concluded that one single step of extraction with 0.03M HCl at 90°C for 4 hours showed optimum results in terms of high fucoidan yield without disrupting the structural integrity of the polymer (Ale, Mikkelsen, et al., 2011a). Recently, Box-Behnken design was used to optimize the pH, temperature and time of application of HCl treatment to a defatted biomass of Ecklonia radiata to obtain a high yield of both fucoidan and alginates and low degradation of alginates, measured by their molecular weight characteristics of each extract obtained (Lorbeer et al., 2015). The same RSM design was applied most recently to optimize the yield and degree of sulphation of fucoidan from
dried-milled *Sargassum* sp. using McIlvaine buffer solution at different temperatures, pH and macroalgae to buffer ratios (Hifney et al., 2016).

### 5. Biological activity and potential health applications of macroalgal polysaccharides

The addition of macroalgae to food resulted in an increase of the health-related properties of the resultant products against different diseases (i.e. obesity, dyslipidaemia, hypertension and diabetes) (Roohinejad et al., 2016). Macroalgal polysaccharides display a wide range of biological properties including antiinflammatory, immunostimulatory, antioxidant, anticoagulant, antimicrobial, antiviral, antipeptic, antiadhesive, antiproliferative, antiapoptosis and antitumour properties (Aspridou, Moschakis, Biliaderis, & Koutsoumanis, 2014; Dore et al., 2013; Huang et al., 2016; Kadam, Tiwari, et al., 2015; Roohinejad et al., 2016; Sweeney et al., 2012; Wijesekara et al., 2011). Table 4 summarised antioxidant, anticancer, anticoagulant and antiinflammatory activities which are among the most widely studied properties of macroalgal derived fucoidan and laminarin in recent times (Cong et al., 2016; Hifney et al., 2016; Wu, Shiu, Hsieh, & Tsai, 2016).

The *in vitro* antioxidant activity of polysaccharides have been determined mainly by 1,1-diphenyl-2-picryl hydrazil (DPPH) radical scavenging, ABTS radical scavenging and ferric reducing antioxidant power (FRAP) assays amongst others (Hifney et al., 2016; Huang et al., 2016). There is a marked relationship between the chemical structure of the macroalgal polysaccharides and their antioxidant activity *in vitro*. Low molecular weight sulphated-polysaccharides showed higher antioxidant activity than high molecular weight polysaccharides in macroalgae (Morya, Kim, & Kim, 2012). Fucoidal fractions containing high levels of total sugars, fucose, and uronic acids showed increased radical scavenging activity while molecules with high degree of sulphation showed high FRAP antioxidant activity (Hifney et al., 2016).
Antiproliferative activity *in vitro* of macroalgal polysaccharides have been demonstrated in a wide variety of cell line cultures. Low molecular weight fucoidan fraction from *Alaria angusta* showed antiproliferative effects against HT 29 and T-47D cell lines, while laminarin fraction showed antiproliferative effects against HT 29 cell lines (Menshova et al., 2015). Fucoidan from *Coccophora langsdorfii* inhibited SK-MEL-5 and SK-MEL-28 melanoma cells (Imbs et al., 2016). Also, fucoidan fractions from *Sargassum fusiforme* showed potent antiangiogenic activities that could be useful in cancer therapy (Cong et al., 2016).

The anticoagulant and antithrombotic activities *in vitro* of macroalgal polysaccharides have been predominantly related to the structure and the degree of sulphation of the polysaccharide (Silva et al., 2010; Wijesinghe & Jeon, 2012). O-sulphated 3-linked α-galactans and 3-O-sulphation at C-3 of 4-α-L-fucose-1 → units (in fucoidan) is mainly responsible for its anticoagulant activity (Dore et al., 2013; Jin et al., 2013; Wijesinghe & Jeon, 2012). These sulphate linked sugar units increased the inhibition of factors Xa, IIa and thrombin with the help of antithrombin and heparin cofactor II in blood coagulation intrinsic pathway (Jin et al., 2013; Wijesekara et al., 2011).

Though both laminarin and fucoidan have shown multiple biological activities in *in vitro* systems, their efficiency and bioavailability in *in vivo* model is not completely explored. *In vivo* studies using β-glucans from *Laminaria digitata*, *Laminaria hyperborea* and *Saccharomyces cerevisiae* in the diet of pigs showed a down-regulation of the expression of inflammatory cytokines in the colon and liver of the animals (Sweeney et al., 2012) and mucin gene expression in the ileum and colon (Ryan et al., 2010; Smith et al., 2010). A down-regulation of pro- and antiinflammatory cytokines (IL-6, IL-17A, IL-1b and IL-10) was reported in the colon of post-weaning pigs supplemented with laminarin (Walsh, Sweeney, O'Shea, Doyle, & O'Doherty, 2013). The animals receiving fucoidan showed a reduction in *Enterobacteriaceae* counts and improved faecal consistency due to the ability of fucoidan to
inhibit the attachment of certain bacterial species in the porcine gastrointestinal tract (Walsh et al., 2013).

The role of the chemical structure of macroalgal polysaccharides and their biological activities in vitro and in vivo is poorly understood to date. It is known that the chemical structure of the macroalgal polysaccharides varied according to factors affecting the macroalgal biomass (i.e. macroalgae species, environment and geographical location) as well as conditions during the extraction and purification of the polysaccharides (i.e. temperature, time). In general, macroalgae is considered a renewable biomass which can be utilized for sustainable polysaccharide production. More research is required to improve extraction and purification techniques of polysaccharides from macroalgae, as well as studies on the chemical structure of the obtained polysaccharides and their promising biological activities both in vitro and in vivo for its future use at industrial scale.

6. Conclusions

Laminarin and fucoidan showed a wide range of biological activities (i.e. anticoagulant, antithrombotic, antiviral, antioxidant and antitumour activities amongst others), with potential use in several markets such as the functional foods and nutraceutical, pharmaceutical and cosmeceutical industries.

There are many extraction and purification techniques available to achieve laminarin and fucoidan with different purity levels. There is a need to optimize the protocols of extraction already available in the literature to improve the yields and to preserve the activities of the extracted polysaccharides, while reducing the time, solvents and energy inputs applied during the extraction processes. Novel extraction technologies such as UAE and EAE showed promising industrial potential in terms of scalability and large sample treatment; however, the high costs associated in terms of machinery, enzyme and energy input are important factors
when considering using these novel techniques at large scale to date. Recent use of dye affinity chromatography techniques and widely used AEC and SEC showed important results not only to achieve high purity levels of polysaccharides but also to isolate and collect different fractions of either laminarin or fucoidan with different chemical structure and biological properties.

The chemical structure of the polysaccharides could also be affected by parameters related with the biology of macroalgae. Due to the fact that the majority of macroalgae currently commercialized in the European market is wild harvested biomass, therefore there is a need to study seasonal differences and its influence on the content and chemical structure of polysaccharides to achieve a better understanding of these compounds and its future exploitation from both wild and cultured harvested macroalgae. In addition, several other challenges (i.e. sustainability of macroalgae supply, automatization/scalability of the employed techniques) must be addressed by researchers to achieve its full potential in terms of commercialization and future industrial applications.

Acknowledgments

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Figure 1. Chemical structure of fucoidan from *Laminaria saccharina* and laminarin from *Laminaria digitata* proposed by Cumashi et al. (2007) and Adamo et al. (2011) respectively.
Figure 2. Schematic diagram of polysaccharide extraction and purification from macroalgal biomass.
**Table 1.** Extraction methods of polysaccharides from different macroalgae species.

<table>
<thead>
<tr>
<th>Macroalgae sp.</th>
<th>Compound of interest</th>
<th>Pre-treatments</th>
<th>Extraction</th>
<th>References</th>
</tr>
</thead>
<tbody>
<tr>
<td>*Silvetia babingtonii, Costaria</td>
<td>Fucoidan</td>
<td>Ethanol (40˚C, 3 h)</td>
<td>HCl (60˚C, pH 2-3, 3 h, 2 times) followed by concentration, dialysis and freeze-dry.</td>
<td>Anastyuk, Imbs, et al. (2012); Anastyuk, Shevchenko, et al. (2012); Anastyuk et al. (2010); Imbs et al. (2016)</td>
</tr>
<tr>
<td><em>costata, Fucus evanescens, Laminaria cichorioides</em></td>
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</tr>
<tr>
<td>*Sargassum henslowian, Fucus</td>
<td>Fucoidan</td>
<td>-</td>
<td>HCl (0.03 M, 90˚C, 4 h) followed by filtration and ethanol (60%) precipitation. The final pellet was freeze-dried.</td>
<td>Ale, Mikkelsen, et al. (2011a)</td>
</tr>
<tr>
<td><em>vesiculosus</em></td>
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<td></td>
<td>Ethanol (80%, at room temperature, 12 h) followed by the same treatment at 70˚C. The pellet was treated twice at room temperature and 70˚C with H$_2$O (7h). The pulled supernatants were treated with CaCl$_2$ (2M, 5 h), centrifuged and the pellet dialyzed (1KDa) and freeze-dried.</td>
<td>Foley et al. (2011)</td>
</tr>
<tr>
<td><em>Ascophyllum nodosum</em></td>
<td>Fucoidan</td>
<td>-</td>
<td>CaCl$_2$ (1%, 85˚C, 4 h) followed by centrifugation (16887g, 20 min). The supernatant was precipitated with ethanol (1 h) and re-precipitated with ethanol (~20˚C, 48 h). The pellets were dialyzed (15 kDa) and freeze-dried.</td>
<td>Kim (2012)</td>
</tr>
<tr>
<td>*Ascophyllum nodosum; Fucus</td>
<td>Laminarin,</td>
<td>-</td>
<td>H$_2$O (90-95˚C, 16 h) followed by filtration and concentration. The extract was precipitated with ethanol, centrifuged and the pellet dehydrated with dimethyl ether.</td>
<td>Vijayabaskar et al. (2012)</td>
</tr>
<tr>
<td><em>vesiculosus</em></td>
<td>galactofucans</td>
<td></td>
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<tr>
<td><em>Sargassum swartzii</em></td>
<td>Sulphated polysaccharides</td>
<td>-</td>
<td>H$_2$O (120˚C, 3 h) followed by filtration and addition of MgCl$_2$ and ethanol (85%) and filtrate again. The new filtrate was dialyzed (3.6 kDa, 24 h), precipitated with ethanol (95%, 3 times). The pellet was dried (80˚C).</td>
<td>J. Wang et al. (2012)</td>
</tr>
<tr>
<td><em>Laminaria japonica</em></td>
<td>Fucoidan</td>
<td>-</td>
<td></td>
<td></td>
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<tr>
<td><strong>Sargassum vulgare</strong></td>
<td>Fucoidan</td>
<td>Acetone</td>
<td>Proteolytic enzyme in NaCl (0.25 M, pH 8, 60°C, 24 h) followed by filtration, precipitation with acetone (0.3, 0.5, 1 and 1.5 volumes) and collect the different precipitates generated by the different volumes to freeze-dry.</td>
<td>Dore et al. (2013)</td>
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<tr>
<td><strong>2 Sargassum sp., 3 red macroalgae</strong></td>
<td>Fucoidan</td>
<td>Methanol : chloroform : water (4:2:1) several times</td>
<td>CaCl$_2$ (2%, 85°C, 24 h, 6 times). The combined supernatants were treated with 10% CH$_3$(CH$<em>2$)$</em>{15}$N(Br)(CH$_3$)$_3$, followed by centrifugation (3000g, 10 min) and the pellet washed several times with H$_2$O and ethanol (20%) and dialyzed (2kDa).</td>
<td>Lim et al. (2014)</td>
</tr>
<tr>
<td><strong>Laminaria hyperborea,</strong>  <strong>Ascophyllum nodosum</strong></td>
<td>Laminarin</td>
<td>-</td>
<td>Sonication 15 min at room temperature with HCl 0.1 M (better yield) and water, followed by centrifugation and precipitation of the supernatant with ethanol (4°C overnight). The mixture was centrifuged and the pellet freeze-dried.</td>
<td>Kadam, O'Donnell, et al. (2015)</td>
</tr>
<tr>
<td><strong>Alaria angusta</strong></td>
<td>Galactofucan</td>
<td>Ethanol 70%, 10 days</td>
<td>HCl (0.1M, 60°C, 2 h, 2 times) followed by centrifugation, dialysis of supernatant and freeze-dry.</td>
<td>Menshova et al. (2015)</td>
</tr>
<tr>
<td><strong>Ascophyllum nodosum</strong></td>
<td>Fucoidan</td>
<td>Ethanol (80%, room temperature, 18 h) and repeat again at 70 °C (4 h)</td>
<td>Microwave treatment (120°C, 15 min) with biomass in HCl (0.1 M). The mixture was dried (80°C), re-dissolved CaCl$_2$ (2%, 4°C, overnight) followed by centrifugation and ethanol precipitation of the supernatant. The new pellet collected after centrifugation was freeze-dried</td>
<td>Yuan and Macquarrie (2015)</td>
</tr>
<tr>
<td><strong>Sargassum fusiforme</strong></td>
<td>Fucoidan</td>
<td>H$_2$O (100°C) followed by concentration and centrifugation. The supernatant was precipitated with ethanol (95%) and the pellet treated with CaCl$_2$ (2%) and freeze dried.</td>
<td>Cong et al. (2016)</td>
<td></td>
</tr>
<tr>
<td>Species</td>
<td>Product(s)</td>
<td>Extraction/Processing Steps</td>
<td>Reference</td>
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<tr>
<td><em>Sargassum swartzii</em></td>
<td>Fucoidan</td>
<td>Soxhlet ethanol-acetone for 24 h, HCl (0.05 M, room temperature, 24 h, 2 times). Supernatants mixed with CaCl₂ (4%, 4°C, overnight) followed by centrifugation and ethanol precipitation of supernatant and dialysis of the pellet.</td>
<td>Dinesh et al. (2016)</td>
<td></td>
</tr>
<tr>
<td><em>Sargassum gaula.ucens</em></td>
<td>Fucoidan</td>
<td>Compressional puffing (0-140-180-220°C) followed by ethanol (1:10, room temperature, 1 h), H₂O (85°C, 1h) followed by centrifugation (3870g, 10 min). The supernatant was precipitated with ethanol (20% to precipitate alginic acid) and then 50% followed by centrifugation and drying (40°C).</td>
<td>Huang et al. (2016)</td>
<td></td>
</tr>
<tr>
<td><em>Coccophora langsdorfii</em></td>
<td>Laminarin, fucoidan and alginates</td>
<td>Ethanol (96%, 40°C, 24 h) and acetone washes, HCl (0.1 M, room temperature, 2 times) and the supernatant neutralized with NaHCO₃ (3%) to pH 5.7-6.1, followed by concentration, dialysis and freeze-dry.</td>
<td>Imbs et al. (2016)</td>
<td></td>
</tr>
<tr>
<td><em>Sargassum</em> sp., <em>Fucus vesiculosus</em>, <em>Ascophyllum nodosum</em>, <em>Lessonia nigrescens</em>, <em>Kjellmaniella crassifolia</em>, <em>Costaria costata</em>.</td>
<td>Fucoidan</td>
<td>Ethanol (95%, 80°C, 4 h, 2 times), H₂O (80°C, 3 h, 3 times), followed by centrifugation (5000 rpm, 10 min). Supernatants were precipitated with ethanol (80%) and the pellet washed in several steps with ethanol-acetone and centrifuged each time until final dialysis and freeze-dry.</td>
<td>Shan et al. (2016)</td>
<td></td>
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</table>
Table 2. Experimental conditions used for the purification of macroalgal polysaccharides with anion-exchange chromatography (AEC).

<table>
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<tr>
<th>Compounds of interest</th>
<th>Experimental conditions</th>
<th>References</th>
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<tbody>
<tr>
<td>Laminarin and fucoidan</td>
<td>DEAE-cellulose column (3.5 × 22 cm, Cl(^{-}) form) equilibrated with 0.05 M HCl. Laminarin eluted with 0.05 M HCl, and fucoidan fractions with 0.5, 1 and 2 M NaCl.</td>
<td>Anastyuk, Imbs, et al. (2012)</td>
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<tr>
<td>Fucoidan</td>
<td>Q-Sepharose Fast Flow column. Eluted with a gradient of 0–3 M NaCl. Flow rate: 3 mL/min.</td>
<td>P. Wang et al. (2012)</td>
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<tr>
<td>Fucoidan</td>
<td>Macro- Prep DEAE column (2.5 × 9 cm, Cl(^{-}) form) equilibrated with 0.1 M NaCl. Eluted with a linear gradient of 0.1-2 M NaCl</td>
<td>Menshova et al. (2015)</td>
</tr>
<tr>
<td>Fucoidan</td>
<td>DEAE-cellulose (50 × 5 cm, Cl(^{-}) form). Eluted stepwise with 0, 0.2, 0.4, 0.8 and 1.6 M NaCl, followed with 0.3 M NaOH</td>
<td>Cong et al. (2016)</td>
</tr>
<tr>
<td>Fucoidan</td>
<td>DEAE cellulose-52 (3 × 30 cm). Eluted with linear gradient 0–1 M NaCl and 0.05 M sodium phosphate buffer solution. Flow rate: 60 mL/h</td>
<td>Dinesh et al. (2016)</td>
</tr>
<tr>
<td>Laminarin and fucoidan</td>
<td>DEAE-cellulose (Fluca) column (3.0 × 14 cm). Eluted first with H(_2)O and the fractions obtained further eluted with a linear gradient 0-2 M NaCl</td>
<td>Imbs et al. (2016)</td>
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</table>
Table 3. Experimental conditions used for the purification of polysaccharides from macroalgae with size-exclusion chromatography (SEC).

<table>
<thead>
<tr>
<th>Compounds of interest</th>
<th>Experimental conditions</th>
<th>References</th>
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<tr>
<td>Fucoidan</td>
<td>Shodex Asahipak GS-520 HQ and Shodex Asahipak GS-620 HQ (7.5 × 300 mm). Eluted with H₂O. Flow rate: 0.8 mL/min.</td>
<td>Imbs et al. (2010)</td>
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<tr>
<td>Fucoidan</td>
<td>TSK G4000 SW-XL (300 x 7.8 mm) and TSK G3000 SW-XL (300 x 7.8 mm). Eluted with 0.1M NH₄OAc acetate. Flow rate: 0.5 mL/min.</td>
<td>Foley et al. (2011)</td>
</tr>
<tr>
<td>Fucoidan</td>
<td>Shodex Asahipak GS-520 HQ and GS-620 HQ (7.5 × 300 mm). Eluted with H₂O. Flow rate: 0.8 mL/min.</td>
<td>Anastyuk, Imbs, et al. (2012)</td>
</tr>
<tr>
<td>Fucoidan</td>
<td>PL aquagel-OH column. Eluted with 0.2 M Na₂SO₄. Flow rate: 0.5 mL/min.</td>
<td>P. Wang et al. (2012)</td>
</tr>
<tr>
<td>Laminarin</td>
<td>TSKgel column G4000PWXL (7.8 x 300 mm) and G5000PWXL (7.8 x 300 mm). Eluted with H₂O. Flow rate: 0.5 mL/min.</td>
<td>Zha et al. (2012)</td>
</tr>
<tr>
<td>Fucoidan</td>
<td>Sepharose CL-4B (140 × 1.8 cm). Eluted with 0.2 M acetic acid.</td>
<td>Dore et al. (2013)</td>
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<tr>
<td>Fucoidan</td>
<td>Sephacryl S-300 column (100 × 2.6 cm). Equilibrated and eluted with 0.2 M NaCl.</td>
<td>Cong et al. (2016)</td>
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<tr>
<td>Fucoidan</td>
<td>Sepharose 6B column (90 × 1.0 cm). Eluted with 100 mM sodium phosphate buffer. Flow rate : 0.6 mL/min.</td>
<td>Dinesh et al. (2016)</td>
</tr>
<tr>
<td>Fucoidan</td>
<td>Superdex 200 (300 × 10 mm). Eluted with 0.2 M NaCl. Flow rate: 0.3 mL/min.</td>
<td>Huang et al. (2016)</td>
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</table>
Table 4. Bioactivities *in vitro* and *in vivo* of marine polysaccharides isolated from macroalgae.

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<th>Biological activity</th>
<th>Macroalgal polysaccharides</th>
<th>Method</th>
<th>References</th>
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<td>Antioxidant <em>in vitro</em></td>
<td>Fucoidan</td>
<td>Total antioxidant, ferric reducing and hydroxyl radical scavenging activities.</td>
<td>Hifney et al. (2016)</td>
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<td></td>
<td>Fucoidan</td>
<td>Ferrous ion-chelating activity, DPPH and ABTS radical scavenging.</td>
<td>Huang et al. (2016)</td>
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<tr>
<td></td>
<td>Fucoidan</td>
<td>DPPH radical scavenging.</td>
<td>Dore et al. (2013)</td>
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<td></td>
<td>Fucoidan</td>
<td>Inhibit growth of HT 29 and T-47D cell lines.</td>
<td>Menshova et al. (2015)</td>
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<tr>
<td></td>
<td>Laminarin</td>
<td>HT 29 cell lines.</td>
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<tr>
<td></td>
<td>Fucoidan</td>
<td>SK-MEL-5 and SK-MEL-28 melanoma.</td>
<td>Imbs et al. (2016)</td>
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<tr>
<td>Anticoagulant <em>in vitro</em></td>
<td>Fucoidan</td>
<td>Thrombin time (TT), prothrombin time (PT) and activated partial thromboplastin time (APTT) coagulation assays.</td>
<td>Dore et al. (2013); Jin et al. (2013)</td>
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<td></td>
<td>Laminarin (laminarin sulphate)</td>
<td>Upon the structural modification (sulphation) with both O-sulphate and N-sulphate groups.</td>
<td>Kadam, Tiwari, et al. (2015)</td>
</tr>
<tr>
<td>Antiinflammatory <em>in vivo</em></td>
<td>Laminarin</td>
<td>Decrease of inflammatory cytokines in colon and liver <em>in vivo</em>.</td>
<td>Sweeney et al. (2012)</td>
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<tr>
<td></td>
<td>Laminarin</td>
<td>Downregulation of IL-6, IL-17A, IL-1b and IL-10 in the colon of post-weaning pigs <em>in vivo</em>.</td>
<td>Walsh et al. (2013)</td>
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</tbody>
</table>